

## Electrocatalysis in Metal Hydride Electrode. II. Hydrogen Electrode Reaction and Related Properties of Group-IB Metal-Coated LaNi<sub>5</sub> Electrodes

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**Synopsis.** Hydrogen storage type electrodes were fabricated from LaNi<sub>5</sub> powder after coating with group-IB metals by an electroless plating method, followed by press moulding. The hydrogen electrode reaction (HER) characteristics and mechanical stability during hydrogen charge/discharge cycles were then studied in 1.0 M (M = mol dm<sup>-3</sup>) NaOH.

Storage type hydrogen/oxidant fuel cells using metal hydrides have been noted for their high energy storage capacities per unit weight.<sup>1)</sup> There are, however, various problems to be solved before their realization, e.g. proper choice of systems with suitable pressure of the hydrogen charge/discharge cycles, prevention of pulverization of the hydrogen absorbing metals or alloys (metal hydrides) during use, etc. Ishikawa et al.<sup>2)</sup> have reported recently that some hydrogen absorbing alloys can be "microcapsulated" with copper deposited by electroless plating so as to prevent the pulverization during repeated hydrogen charge/discharge cycles and that their hydrogen storage ability after the plating was maintained at the level comparable with those of the untreated alloys. We have reported elsewhere<sup>3)</sup> that the electrocatalyst such as Pt or Ag, which possesses the greater rate of the Volmer over that of the Tafel step, namely the greater  $m_o (=i_{oV}/i_{oT})$  value, is desirable as a surface modifier in the metal hydride electrode from the viewpoint of the energy efficiency in the charge/discharge cycles.

In this work, LaNi<sub>5</sub> powder was microcapsulated with a group-IB metal, and the electrochemical property in alkaline solution was investigated, together with their mechanical stability.

### Experimental

**Preparation of the Electrodes.** LaNi<sub>5</sub> powder (particle size about 100  $\mu$ m and the BET surface area 0.5 m<sup>2</sup> g<sup>-1</sup>) was subjected to electroless plating of Cu or Ag from conventional solutions,<sup>4)</sup> or of Au by immersion of the powder in 2.5 $\times$ 10<sup>-3</sup> M tetrachloroauric (III) acid solution. Amount of the deposition in weight (mol) % was 12.5 (48.6) for Cu, 12.5 (36.4) or 25 (57.2) for Ag, and 25 (42.3) for Au, respectively.

The microcapsulated LaNi<sub>5</sub> powder was pelletized into discs (13 mm diameter $\times$ 1 mm thickness) with use of Ni nets (200 mesh) as electric leads under a static pressure of 400 Kg cm<sup>-2</sup> and then heated at 770 K in vacuo (5 $\times$ 10<sup>-4</sup> Pa) for several hours. The LaNi<sub>5</sub> samples bound with PTFE [poly(tetrafluoroethylene)] emulsion were prepared according to the method described in the literature.<sup>5)</sup> In some

occasions, a small amount of Pt was further deposited electrochemically. The nickel nets were spot-welded to Ta wires which were in turn sealed into Pyrex glass tubings.

**Electrochemical Measurements.** Galvanostatic polarization studies<sup>6)</sup> were carried out in 1.0 M NaOH at 303 K. Real surface area of the test electrode was evaluated from the double layer capacitance data assuming a value of 18  $\mu$ F cm<sup>-2</sup> (true).

### Results and Discussion

**HER Characteristics.** A series of microcapsulated LaNi<sub>5</sub> electrodes showed stable electrochemical behaviors in a similar manner as bare LaNi<sub>5</sub> electrodes. Thus, a typical plateau region was clearly observed on their short time (a few seconds) galvanostatic overpotential rise or decay transient curves respectively before the attainment of the steady-state polarization or of equilibrium potential. Through these observations, the electrodes are judged to possess a good hydrogen absorbability. Hence, as discussed previously,<sup>6-8)</sup> we could estimate two overpotential components,  $\eta_1$  and  $\eta_2'$ , for the water discharge step and the hydrogen adatom recombination step, respectively.

The Tafel plots of  $\eta_1$  on these microcapsulated electrodes showed a basic symmetry between the anodic and cathodic branches and the slope of the linear portion was reasonably close to 120 mV decade<sup>-1</sup>. This indicates that  $\eta_1$  represents the component overpotential for an one electron transfer reaction, namely the Volmer step. Its exchange current density ( $i_{oV}$ ) estimated from the linear plots of  $\eta_1$  vs.  $i$ , the applied current, near the reversible HER potentials was as follows: Cu/LaNi<sub>5</sub> 5.9, Ag/LaNi<sub>5</sub> 9.8, and Au/LaNi<sub>5</sub> 3.7 $\times$ 10<sup>-6</sup> A cm<sup>-2</sup> (true).

On the other hand, the "Tafel lines" of  $\eta_2'$  in the cathodic region gave a slope of ca. 30 mV decade<sup>-1</sup>, except in the region of very high current density where the slope became lower, and indicated that  $\eta_2'$  should be attributed to the Tafel step. The linear  $\eta_2'$  vs.  $i$  plots in the low overpotential region resulted in the following  $i_{oT}$  values: Cu/LaNi<sub>5</sub> 0.7, Ag/LaNi<sub>5</sub> 0.8, and Au/LaNi<sub>5</sub> 0.6 $\times$ 10<sup>-6</sup> A cm<sup>-2</sup> (true), which were roughly one order of magnitude smaller than the corresponding  $i_{oV}$  values. The values of  $i_{oV}$ ,  $i_{oT}$ , and  $m_o (=i_{oV}/i_{oT})$  estimated of the microcapsulated LaNi<sub>5</sub> electrodes are schematically summarized in Fig. 1, together with those observed on some Ni-based alloys<sup>6-8)</sup> and PTFE-bound or Pt-modified LaNi<sub>5</sub> electrodes.

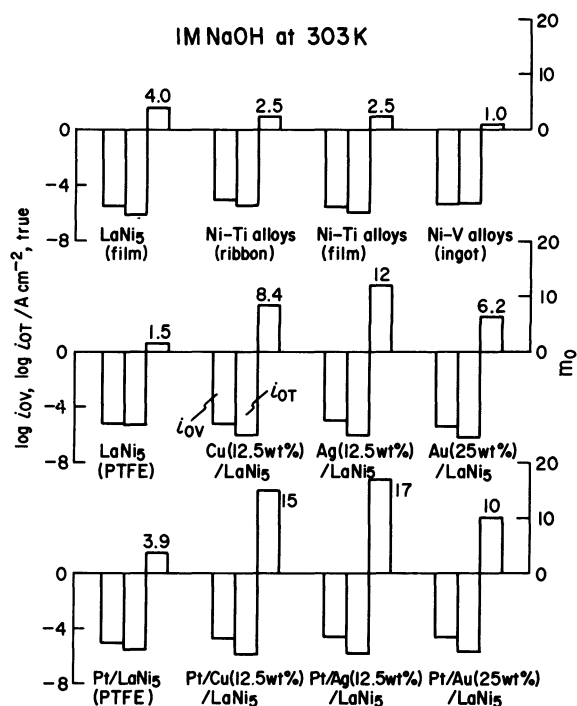


Fig. 1. Schematic diagram of the kinetic data obtained on Ni-based alloy ribbon or film electrodes, LaNi<sub>5</sub> electrodes coated with a series of group-IB metals, those further with Pt, and LaNi<sub>5</sub> electrodes bound with PTFE. 1.0 M NaOH, 303 K.

Table 1. Activation Energies for the Volmer and Tafel Steps and the Overall Reaction on Ni-Based Electrodes

Electrode	$\Delta E/\text{kcal mol}^{-1}$		
	$i_{0V}$	$i_{0T}$	$i_0$
Cu/LaNi <sub>5</sub>	9.0	4.5	4.6
Ag/LaNi <sub>5</sub>	8.9	4.4	4.8
Au/LaNi <sub>5</sub>	8.8	5.1	5.9

It was found that the microcapsulated LaNi<sub>5</sub> electrodes possessed much larger  $m_0$  values (6–12) than those (1–4) of the bare Ni-based alloys. Furthermore, they were considerably larger than those<sup>3)</sup> observed on the group-IB metal electrocatalysts themselves. The larger  $m_0$  values were mainly caused by increased rates of the Volmer step and might indicate the existence of a synergistic effect between LaNi<sub>5</sub> and group-IB metals. A further increase up to  $m_0=17$  was observed after a deposition of Pt on their surface. The PTFE-bound LaNi<sub>5</sub> electrode was mechanically very stable but the  $m_0$  value was relatively small ( $m_0=1.5$ ): No polarization

behaviors for HER could be studied with acceptable reliability, however, as hydrogen bubbles tightly adhered to the PTFE surface.

**Mechanical Stability.** The microcapsulated LaNi<sub>5</sub> electrodes prepared in this work were found to be stable even under polarizations up to  $\eta=-300$  mV for a few ten hours. This was in agreement with the results reported on the hydrogen absorption/desorption cycles in gas phase<sup>2)</sup> or in electrochemical system<sup>9)</sup> of Cu-coated LaNi<sub>5</sub> specimens prepared in a similar manner as in this work. The electrodes were, however, damaged during polarizations over much longer durations even at potentials less than  $-300$  mV.

**Temperature Dependence.** The activation heats evaluated from the Arrhenius plots of  $i_{0V}$ ,  $i_{0T}$ , and  $i_0$  observed on the microcapsulated LaNi<sub>5</sub> electrodes are summarized in Table 1. The values were around 9 and 5 kcal<sup>†</sup> mol<sup>-1</sup> for the Volmer and the Tafel step, respectively, and were in rough agreement with those observed on other Ni-based alloy electrodes.<sup>6–8)</sup> Since the difference between the activation heats of two elementary reaction steps is appreciable (about 4 kcal mol<sup>-1</sup>),  $m_0$  should significantly be increased at higher temperatures. This means that the energy efficiency may be improved if the hydrogen storage cells are operated at higher temperatures, but probably with the cost of decrease of the storage capacity.

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<sup>†</sup> 1 cal=4.18 J.